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(54) **Improved wet laid bonded fibrous web containing bicomponent fibers including LLDPE**

Verbessertes, nassgelegtes, gebundenes Vlies, zweikomponentige Fasern einschliesslich LLDPE
enthaltend

Nappe améliorée non tissée liée formée humide contenant fibres bi-composants LLDPE inclus

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EP-A- 0 279 511 **FR-A- 2 596 075**
GB-A- 2 125 458 **GB-A- 2 127 866**

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DescriptionBackground of the Invention5 1. Field of the Invention

The present invention relates to a thermally bonded fibrous wet laid web containing a specific bicomponent fiber. This thermally bonded fibrous wet laid web not only has increased web strength, but also is found to provide greater web uniformity. Furthermore, the web is found to be much softer than a regular paper web. In particular, the bicomponent
 10 fiber consists essentially of a first component consisting of polyester or polyamide and a second component consisting of linear low density polyethylene. The thermally bonded fibrous wet laid web may further include a matrix fiber selected from a group consisting of cellulose paper making fibers, cellulose acetate fibers, glass fibers, polyester fibers, ceramic fibers, metal fibers, mineral wool fibers, polyamide fibers, and other naturally occurring fibers.

15 2. Prior Art

In the prior art processes of making wet laid webs or paper from fibers of whatever source, it is customary to suspend previously beaten fibers, or what is generally known as pulp, in an aqueous medium for delivery to a sheet-forming device, such as a Fourdrinier wire. This fiber-containing aqueous dispersion is commonly referred to in the art as a
 20 furnish. One troublesome problem at this stage of making wet laid fibrous webs, is the tendency for the fibers to clump, coagulate or settle in the aqueous vehicle. This condition is generally referred to as flocculation, and greatly impedes the attainment of uniform web formation. That is, flocculation causes a nonuniform distribution of fibers in the paper product produced therefrom and manifests not only a mottled, uneven appearance, but is also defective in such important physical properties as tear, burst, and tensile strength. Another problem in making wet laid fibrous webs is a tendency
 25 of the fibers to float to the surface of the furnish.

For the manufacture of fibrous wet laid webs from conventionally used fibers such as cellulose, methods are known for attaining uniform dispersion of the fibers and reducing and even preventing the occurrence of flocculation. One of the more effective means has been to add a small amount of karaya gum to the fiber furnish. However, this has proved unsuccessful in various applications but other agents such as carboxymethyl cellulose or polyacrylamide have been
 30 used to attain the desired result of the cellulose in the furnish.

Fibrous wet laid webs may also be made from other natural or synthetic fibers in addition to the wood cellulose paper-making fibers. A water furnish of the fibers is generally made up with an associative thickener and a dispersant. The cellulose pulp is dispersed in water prior to adding the dispersant, followed by the addition of the associative thickener in an amount in the range up to 150 pounds per ton of dry fiber making up the water furnish and then the addition and
 35 dispersion of the natural and/or synthetic fibers. Finally, the dispersion of mixed fibers in a water carrier is diluted to the desired headbox consistency and dispensed onto the forming wire of a conventional paper-making machine. An anti-foam agent may be added to the dispersion to prevent foaming, if necessary, and a wetting agent may be employed to assist in wetting the fibers if desired. A bonded fibrous web may be formed from the fiber furnish on a high speed conventional Fourdrinier paper making machine to produce a strong, thermally bonded fibrous wet laid web.

In prior art processes for wet lay wherein the textile staple fibers are polyester fibers, water-based binders are generally added to the process to insure adhesion between the cellulose fibers and the polyester fibers. Generally, from about 4% to about 35% binder material is employed. One of the problems encountered using a water based binder is the binder leaches out of the resultant web in such applications as filters. Addition of binders increases cost and results in environmental problems. Furthermore, latex binders have a short shelf life and require special storage conditions.
 40 Also, the latex binders may be sensitive to the condition of the diluent water employed.

It is well known to blend bicomponent fibers with natural and synthetic fibers in dry processes of making nonwoven fabrics. For example, in European Patent Application No. 0 070 164 to Fekete et al there is disclosed a low density, high absorbent thermobonded, nonwoven fabric comprising a staple length polyester/polyethylene bicomponent fiber and short length natural cellulose fibers. The U. S. Patent No. 4,160,159 to Samejima discloses an absorbent fabric containing wood pulp combined with short-length, heat fusible fibers. Although these patents disclose the use of the combination of bicomponent fibers and cellulose fibers, the disclosure is not directed to a wet lay application. Many problems arise in attempting to incorporate a heat fusible fiber such as a bicomponent fiber into a wet lay fibrous web.
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Such nonwoven textile fabrics are normally manufactured by laying down one or more fibrous layers or webs of textile length fibers by dry textile carding techniques which normally align the majority of the individual fibers more or less generally in the machine direction. The individual textile length fibers of these carded fibrous webs are then bonded by conventional bonding (heating) techniques, such as, for example by point pattern bonding, whereby a unitary, self-sustaining nonwoven textile fabric is obtained.
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Such manufacturing techniques, however, are relatively slow and it has been desired that manufacturing processes

having greater production rates be devised. Additionally, it is to be noted that such dry textile carding and bonding techniques are normally applicable only to fibers having a textile cardable length of at least about 1.27 cm (1/2 inch) and preferably longer and are not applicable to short fibers such as wood pulp fibers which have very short lengths of from about 0.42 cm (1/6 inch) down to about 0.10 cm (1/25 inch) or less.

More recently, the manufacture of nonwoven textile fabrics has been done by wet forming technique on conventional or modified paper making or similar machines. Such manufacturing techniques advantageously have much higher production rates and are also applicable to very short fibers such as wood pulp fiber. Unfortunately, difficulties are often encountered in the use of textile length fibers in such wet forming manufacturing techniques.

Problems encountered in attempting to incorporate a heat fusible fiber such as a bicomponent fiber into a wet lay process is attaining uniform dispersion of the bicomponent fiber as well as attaining a thermally bonded web with sufficient strength such that the thermally bonded web is usable. It has been found in the past that bicomponent fibers containing a sheath of high density polyethylene (HDPE) and a core of polyester are difficult to uniformly disperse in wet lay solutions. When dispersion of fibers has been attained, fibrous webs produced therefrom have been found to have lacked the desired strength.

European Patent Application 0 311 860 discloses a bicomponent fiber having a polyester or polyamide core and a sheath component consisting of a copolymer straight-chain low density polyethylene; and the bicomponent fiber can be formed into a web through the use of known methods of making nonwoven fabrics including wet laying. The copolymer polyethylene is defined as consisting of ethylene and at least one member selected from the class consisting of an unsaturated carboxylic acid, a derivative from said carboxylic acid and a carboxylic acid and a carboxylic acid anhydride. The application fails to provide any details regarding the copolymer polyethylene into a wet lay process or the resulting properties of the web produced therefrom.

GB-A-2 125 458 discloses a thermally bonded fibrous web consisting essentially of a bicomponent fiber comprising a polyester or polyamide component and a second component consisting essentially of a linear low density polyethylene having a density in the range of 0.910 to 0.940 g/cc. The web may also include a matrix fiber.

There remains a need to develop a thermally bonded wet lay fibrous web including a suitable heat fusible bicomponent filament which will not only increase the strength of the web, but also avoid problems associated with adding binders.

The present invention is directed to a thermally bonded fibrous wet laid web including a specific bicomponent fiber so as to yield a thermally bonded web not only having increased strength, but also greater web uniformity and softer than a regular paper web. In particular, the thermally bonded fibrous wet laid web of the present invention consists essentially of a bicomponent fiber comprising a first fiber component of polyester or polyamide, and a second component consisting essentially of a linear low density polyethylene (LLDPE) having a density in the range of 0.88 g/cc to 0.945 g/cc and a grafted high density polyethylene (HDPE) having initially a density in the range of 0.94 g/cc to 0.965 g/cc, which has been grafted with maleic acid or maleic anhydride, thereby providing succinic acid or succinic anhydride groups grafted along the HDPE polymer.

Furthermore, the present invention includes a thermally bonded fibrous wet laid web comprising a bicomponent fiber consisting essentially of a first component of polyester or polyamide, and a second component consisting essentially of a linear low density polyethylene having a density in the range of 0.88 g/cc to 0.945 g/cc and a grafted high density polyethylene (HDPE) having initially a density in the range of 0.94 g/cc to 0.965 g/cc, which has been grafted with maleic acid or maleic anhydride, thereby providing succinic acid or succinic anhydride groups grafted along the HDPE polymer chain; and a matrix fiber selected from the group consisting essentially of cellulose paper making fibers, cellulose acetate fibers, glass fibers, polyester fibers, ceramic fibers, mineral wool fibers, polyamide fibers and other naturally occurring fibers.

Brief Description of the Drawings

Figure 1 shows a graph illustrating the relationship of tensile strength to various levels of bicomponent fibers in a thermally bonded web as described in Example 2.

Figure 2 shows a graph illustrating the relationship of elongation to various levels of bicomponent fibers in a thermally bonded web as described in Example 2.

Figure 3 shows a graph illustrating the relationship of the Elmendorf tear tests to various levels of bicomponent fibers in a thermally bonded web as described in Example 2.

Figure 4 shows a graph illustrating the relationship of the Mullen Burst test to various levels of bicomponent fibers in a thermally bonded web as described in Example 2.

Description of the Preferred Embodiments

A thermally bonded fibrous wet laid web of the present invention is prepared from a specific bicomponent fiber and

optionally a matrix fiber. Processes to make such thermally bonded fibrous wet laid web would also use suitable dispersant and thickeners.

Bicomponent fibers suitable for the present invention include a first component or a backbone polymer of polyester or polyamide or polypropylene. Polyester, polyamides and polypropylene are well known textile materials used in the manufacture of fabrics and other applications. Although polyester and polyamides have been listed, any suitable backbone polymer would include polymers having a higher melting point than the LLDPE. Generally the backbone polymer has a melting point at least 30°C higher than that of the second component.

Also included in the bicomponent fiber is a second component consisting essentially of a linear low density polyethylene. Such polymers are termed "linear" because of the substantial absence of branched chains of polymerized monomer units pendant from the main polymer "backbone". It is these linear polymers to which the present invention applies. In some, there is a "linear" type ethylene polymer wherein ethylene has been copolymerized along with minor amounts of alpha, beta-ethylenically unsaturated alkenes having from 3 to 12 carbons per alkene molecule, preferably 4 to 8. The amount of the alkene comonomer is generally sufficient to cause the density of the polymer to be substantially in the same density range of LDPE, due to the alkyl sidechains on the polymer molecule, yet the polymer remains in the "linear" classification; they are conveniently referred to as "linear" low density polyethylene.

The LLDPE polymer may have a density in the range of about 0.88 g/cc to about 0.945 g/cc, preferably about 0.90 g/cc to about 0.940 g/cc. It is evident to practitioners of the relevant arts that the density will depend, in large part, on the particular alkene(s) incorporated into the polymer. The alkenes copolymerized with ethylene to make LLDPE comprises a minor amount of at least one olefinically unsaturated alkene of the form $C_3 - C_{12}$, most preferably from $C_4 - C_8$; 1-octene is especially preferred. The amount of said alkene may constitute about 0.5% to about 35% by weight of the copolymer, preferably about 1% to about 20%, most preferably about 1% to about 10%.

The LLDPE polymer may have a melt flow value (MFV) in the range of about 5 gm/10 min to about 200 gm/10 min as measured in accordance with ASTM D-1238(E) at 190°C. Preferably the melt flow value is in the range of about 7 gm/10 min to about 120 gm/10 min, most preferably about 10 gm/10 min to about 105 gm/10 min. Practitioners of the relevant arts are aware that the melt flow value is inversely related to the molecular weight of the polymer.

The second component of the bicomponent fiber also include a grafted high density polyethylene (HDPE), in a blend with the LLDPE wherein the HDPE has been grafted with maleic acid or maleic anhydride, thereby providing succinic acid or succinic anhydride groups grafted along the HDPE polymer chain. The HDPE for use in the present invention is a normally solid, high molecular weight polymer prepared using a coordination-type catalyst in a process wherein ethylene is homopolymerized. The HDPE which is used in making the grafted HDPE in accordance with the present invention is characterized as having a melt flow value in the range of about 5 g/10 min to about 500 g/10 min according to ASTM D-1238(E) at 190°C and a density in the range of about 0.94 g/cc to about 0.965 g/cc, preferably a MFV about 7 gms/10 min to about 150 gms/10 min and a density of about 0.945 g/cc to about 0.960 g/cc. The anhydride or acid groups generally comprise about 0.0001 to about 10 wt. percent, preferably about 0.01 to about 5 wt. percent of the HDPE. The ratio of grafted-HDPE/ungrafted LLDPE of the present blend is in the range of about 2/98 to about 30/70, preferably about 5/95 to about 20/80.

The maleic acid and maleic anhydride compounds are known in these relevant arts as having their olefin unsaturation sites conjugated to the acid groups, in contradistinction to the fused ring and bicyclo structures of the non-conjugated unsaturated acids of e.g., U. S. Pat. No. 3,873,643 and U. S. Pat. No. 3,882,194 and the like. Fumaric acid, like maleic acid of which it is an isomer, is also conjugated. Fumaric acid, when heated rearranges and gives off water to form maleic anhydride, thus is operable in the present invention. Other alpha, beta unsaturated acids may be used.

The grafting of the succinic acid or succinic anhydride groups onto ethylene polymer may be done by methods described in the art, which involve reacting maleic acid or maleic anhydride in admixture with heated polymer, generally using a peroxide or other free-radical initiator to expedite the grafting.

Grafting may be effected in the presence of oxygen, air hydroperoxides, or other free radical initiators, or in the essential absence of these materials when the mixture of monomer and polymer is maintained under high shear in the absence of heat. A convenient method for producing the graft copolymer is the use of extrusion machinery, however, Banbury mixers, roll mills and the like may also be used for forming the graft copolymers.

Another method is to employ a twin-screw devolatilizing extruder (such as a Werner-Pfleider twin-screw extruder) wherein maleic acid (or maleic anhydride) is mixed and reacted with the HDPE at molten temperatures, thereby producing and extruding the grafted polymer. The so-produced grafted polymer is then blended, as desired, with LLDPE to produce the blends of this invention.

Manufacture of bicomponent filaments of either the sheath/core configuration or the side-by-side configuration by the use of spinning packs and spinnerets is well known in the art. A conventional spinning process for manufacturing a fiber with a sheath/core configuration involves feeding the sheath-forming material to the spinneret orifices in a direction perpendicular to the orifices, and injecting the core-forming material into the sheath-forming material as it flows into the spinneret orifices. Reference is made to U. S. Patent Nos. 4,406,850 and 4,251,200 which discloses bicomponent spinning assemblies and describe the production of bicomponent fibers. These patents are incorporated by reference.

Bicomponent fibers of the present invention may be either eccentric or concentric. It is understood, however, that the bicomponent fibers having side-by-side configurations or multi-segmented bicomponent fibers are also considered to be within the scope of the present invention.

It has been found that such bicomponent fibers generally have a length to diameter ratio of between about 100:1 and about 2000:1. Such lengths are generally found to be about 1 mm to about 75 mm and preferably about 10 mm to 15 mm long. Diameters of the fibers are from about 0.5 dpf to about 50 dpf. Such bicomponent fibers are generally cut on conventional process machines well known in the art.

The second ingredient that may be used in the present invention is the matrix fibers. Such fibers can be generally characterized by the fact that all these fibers provide chemical bonding sites through hydroxyl or amine groups present in the fiber. Included in the class of such matrix fibers are the cellulose paper making fibers, cellulose acetate fibers, glass fibers, polyester fibers, metal fibers, ceramic fibers, mineral wool fibers, polyamide fibers, and other naturally occurring fibers.

In the process for dispersing the bicomponent fibers and matrix fibers in a furnish, a whitewater system of water, thickener and dispersant is employed. The dispersant acts first to separate fibers and wet out the surface of the fibers. The thickener acts to increase the viscosity of the water carrier medium and also acts as a lubricant for the fibers. Through these actions, the thickener acts to combat flocculation of the fibers.

Various ingredients may be used as a thickener. One class of nonionic associative thickeners comprise relatively low (10,000 - 200,000) molecular weight ethylene oxide based urethane block copolymers and are disclosed in U. S. Patent Nos. 4,079,028 and 4,155,892, incorporated herein by reference. These associative thickeners are particularly effective when the fiber furnish contains 10% or more staple length hydrophobic fibers. Commercial formulations of these copolymers are sold by Rohm and Haas, Philadelphia, PA, under the trade names ACRY SOL RM-825 and ACRY SOL RHEOLOGY MODIFIER QR-708, QR-735, and QR-1001 which comprise urethane block copolymers into carrier fluids. ACRY SOL RM-825 is 25% solids grade of polymer in a mixture of 25% butyl carbitol (a diethylene glycol monobutylether) and 75% water. ACRY SOL RHEOLOGY MODIFIER QR-708, a 35% solids grade in a mixture of 60% propylene glycol and 40% water can also be used.

Similar copolymers in this class, including those marketed by Union Carbide Corporation, Danbury, Conn. under the trade names SCT-200 and SCT-275 and by Hi-Tek Polymers under the trade name SCN 11909 are useful in the process of this invention. Other thickeners include modified polyacrylamides available from Nalco Chemical Company.

Another class of associative thickeners, preferred for making up fiber furnishes containing predominantly cellulose fibers, e.g. rayon fibers or a blend of wood fibers and synthetic cellulosic fibers such as rayon comprises modified nonionic cellulose ethers of the type disclosed in U. S. Patent No. 4,228,277 incorporated herein by reference and sold under the trade name AQUALON by Hercules Inc., Wilmington, Delaware. AQUALON WSP M-1017, a hydroxy ethyl cellulose modified with a C-10 to C-24 side chain alkyl group and having a molecular weight in the range of 50,000 to 400,000 may be used in the whitewater system.

The dispersing agents that may be used in the present invention are synthetic, long-chain, linear molecules having an extremely high molecular weight, say on the order of at least 1 million and up to about 15 million, or 20 million, or even higher. Such dispersing agents are oxygen-containing and/or nitrogen-containing with the nitrogen present, for example, as an amine. As a result of the presence of the nitrogen, the dispersing agents have excellent hydrogen bonding properties in water. The dispersing agents are water soluble and very hydrophilic.

It is also believed that these long chain, linear, high molecular weight polymeric dispersing agents are deposited on and coat the fiber surface and make it slippery. This development of excellent slip characteristic also aids in deterring the formation of clumps, tangles and bundles. Examples of such dispersant agents are polyethylene oxide which is a nonionic long chain homopolymer and has an average molecular weight of from about 1 million to about 7 million or higher; polyacrylamide which is a long straight chain nonionic or slightly anionic homopolymer and has an average molecular weight of from about 1 million up to about 15 million or higher, acrylamide-acrylic acid copolymers which are long, straight chain anionic polyelectrolytes in neutral and alkaline solutions, but nonionic under acid conditions, and possess an average molecular weight in the range of about 2 - 3 million, or higher; polyamines which are long straight chain cationic polyelectrolytes and have a high molecular weight of from about 1 million to about 5 million or higher; etc. A preferred dispersant is an oxyalkylated fatty amine. The concentration of the dispersing agents in the aqueous media may be varied within relatively wide limits and may be as low as 1 ppm and up to as high as about 200 ppm. Higher concentrations up to about 600 ppm may be used but tend to become uneconomical due to the cost of the dispersing agent and may cause low wet web strength. However, if recovering means is provided whereby the aqueous medium and the dispersing agent therein is recycled and reused, then concentrations up to 1,000 ppm or even higher can result.

The fiber concentration in the fiber slurry may also be varied within relatively wide limits. Concentrations as low as about 0.1% to 6.0% by weight of the furnish are suitable. Lighter or heavier ranges may be employed for special products intended for special purposes.

It has been found that the bicomponent and matrix fibers may be equally dispersed through an aqueous medium by adding a suitable dispersing agent and thickener to the resulting fiber slurry stirring and agitation of the slurry. The

dispersing agent is added to the aqueous medium first and then the bicomponent fibers followed by the thickener and the matrix fibers are subsequently added thereto. The individual bicomponent fibers and matrix fiber are dispersed in the furnish uniformly through stirring with a minimum amount of fiber flocculation and clumping.

It is believed that by so doing the fibers enter a favorable aqueous environment containing the dispersing agent which is immediately conducive to their maintaining their individuality with respect to each other whereby there is substantially no tendency to flocculate or form clumps, tangles or bundles. This, of course, is to be contrasted to the prior situation wherein when bicomponent fibers are initially placed in an unfavorable aqueous environment not containing any high molecular weight, linear polymeric, water soluble, hydrophilic dispersing agent, which environment is conducive to the loss of fiber individuality whereby the fibers flocculate and form clumps, tangles, and bundles and tend to migrate either to the top or the bottom of the furnish.

It has been found that specific types of dispersing agents are required in dispersing the bicomponent fibers of the present invention to arrive at the conditions of nonflocculation.

After the wet laid web has been formed, excess water is removed from the web by passing the web over a suction slot. Then the web is dried and thermally bonded by passing the web through a drying machine raised to sufficient temperature to melt the second component of the bicomponent fiber which then acts as an adhesive to bond the bicomponent fiber to other bicomponent fibers and matrix fibers upon cooling. One such machine is a Honeycomb System Through-air Dryer. The heating temperature may be from 140°C to 220°C, preferably 145°C to 200°C. The thermally bonded web is then cooled with the adhesive bonds forming at below the resolidification of the second component.

The invention will be described in greater detail in the following examples wherein there are disclosed various embodiments of the present invention for purposes of illustration, but not for purposes of limitation of the broader aspects of the present inventive concept.

Experimental Procedure

A. Bicomponent Fibers

Bicomponent fibers were made having a substantially concentric sheath/core configuration. The core was made from a standard 0.64 IV semi-dull polyethylene terephthalate. The sheath was made from a polymer described for the specific bicomponent fiber.

Bicomponent fiber A was made having a sheath of linear low density polyethylene containing from 1 - 7% 1-octene wherein the polymer had a density of 0.930 g/cc, a melt flow value of 18 gm/10 min at 190°C according to ASTM D-1236 (E). Such a LLDPE is commercially available from Dow Chemical Company or Aspun Resin 6813.

Bicomponent fiber B was made having a sheath made from a blend of LLDPE and grafted HDPE wherein the blend had a density of .932 g/cc and a melt flow value of 16 gm/10 min at 190°C. The HDPE was grafted with maleic anhydride to contain 1 wt.% succinic anhydride groups. This sheath material is described in U. S. Patent No. 4,684,576. The ratio of grafted HDPE/LLDPE was 10/90.

Each type of the bicomponent fibers were made by coextruding the core and sheath polymers, and drawing the resulting filaments by processes well known to those skilled in the art, to obtain the desired denier and sheath/core ratio. The bicomponent fibers were cut to have a length of about 0.5 inch.

B. Wet Lay Process

A batch fiber-water furnish was made with 500 liters of water at an ambient temperature in a mix tank equipped with an agitator rotating at 500 rpm. To the furnish was added in the following order:

- a) 20 ml of the dispersing agent Milese T which is commercially available from ICI Americas, Wilmington, Delaware;
- b) 250 grams of the selected bicomponent fibers;
- c) 1 liter of 1% solution having a solids content of 35% of the viscosity modifier Nalco 061 commercially available from Nalco Chemical Company, Naperville, Illinois;
- d) 15 ml of a dispersant for a matrix fiber such as glass fibers Katapol VP532SPB commercially available from GAF Corporation located in New York, New York; and
- e) 250 grams of a matrix fiber pursuant to the experiment.

Prepared in a separate tank with an agitator was a white water solution containing 1100 liters of water, 40 ml of

Milese T, and 2 liter of 1% solution Nalco 061. The furnish and the white water solution were both pumped to the headbox of a wireformer. Pump rates were 24 l/min of the furnish and 30 l/min of the white water to give a .044% consistency, i.e. grams of fiber to water.

Once the web was formed, it is then dried and thermally bonded thereafter to produce a thermally bonded fibrous web. The bonded web was then tested for such properties including tensile strength, tear strength, elongation and Mullen Burst and the strength tests were done in the machine direction (MD) and the cross direction (CD). The tensile strength test is used to show the strength of a specimen when subjected to tension wherein a 1 inch wide sample by 7 inches long was pulled at 12 inch/min with a 5 inch jaw space. Elongation is the deformation in the direction of the load caused by tensile force and the reading is taken at the breaking load during the tensile test. The tear tester used was an Elmendorf Tear Tester which is a tester designed to determine the strength of the thermally bonded wet laid fabric. The Mullen Burst Test is an instrumental test method that measure the ability of a fabric to resist rupture by pressure exerted by an inflated diaphragm.

Example 1

Wet laid webs were made up of bicomponent fibers and glass fibers and thermally bonded at 204°C into a thermally bonded web. The thermally bonded web was tested to demonstrate the present invention and compare it to a wet laid web made using a commercially available HDPE/PET bicomponent fiber.

The glass fibers are made from silica base, having a thickness of 15 microns and a length of 12,7 cm (0.5 inch). Such fibers are commercially available from Grupo Protexa, Mexico. The ratio of bicomponent fibers to glass fibers was 50/50. The bicomponent fibers and glass fibers were added to the water furnish as described in the wet lay process.

In Experiment 1 (the control), a bicomponent fiber was used having a PET core and a HDPE sheath, wherein the sheath/core ratio was 50/50 and the fiber has a denier of 2 dpf and a cut length of 3/8 inches. Such bicomponent fibers are commercially available as K-56 fiber type from Hoechst Celanese Corporation.

Experiment 2 was similar to Experiment 1, but the bicomponent fiber was replaced with bicomponent fiber A having sheath/core ratio of 50/50, a denier of 2 dpf, and a cut length of (0.5 inches) 12,7 cm.

Experiment 3 was similar to Experiment 1 and 2, but the bicomponent fiber used was bicomponent fiber B having a denier of 3 dpf, a cut length of 12,7 cm (0.5 inches) and a sheath core ratio of 50/50.

The webs were tested for the tensile strength and tear strength in both the machine direction and cross direction. Also, the webs were tested for the Mullen Burst test. The results of the example are set forth in Table 1.

Table 1

	g/cm	TENSILE		g/cm	ELMENDORF TEAR		kPa	Basis Weight g/m ²
		MD	CD		MD	CD		
Experiment 1	37	(2.09)	(2.15)	38	217.3	213.3	(7.3)503	(1.16)39.3
Experiment 2	57.2	3.23	(3.76)	66.6	357.3	305.3	(10.1)697	(1.14)38.7
Experiment 3	75.6	(4.27)	(4.47)	79	313.3	297.3	(10.3)711	(1.21)41.0

Tensile values are in lbs./in.

Tear values are in grams and is an Elmendorf tear.

Mullen values are in PSI.

MD - Machine Direction

CD - Cross Direction

Base Weight is in oz/yd².

Thermally bonded wet laid web produced in Experiment 1 was the control using a prior art bicomponent fiber of a HDPE sheath and PET core. It's tensile strength was 37g/cm (2.09 lbs./in). in the machine direction, 38 g/cm (2.15 lbs./in) in the cross direction; the tear strength was 217.3 grams in the machine direction and 213.3 grams in the cross direction; and the Mullen Burst test value of 503 kPa (7.3 PSI).

Experiment 2 demonstrates that by replacement of the prior art HDPE/PET bicomponent fiber with bicomponent fiber A in the wet laid web of the present invention, the tensile strength and tear strength in both the machine and cross directions significantly increase as does the Mullen Burst Test value which indicates improved adhesion of the bicomponent fiber to the glass fiber in this case. In fact, the strength increase is about 50% over the control.

Experiment 3 demonstrates that employing a bicomponent fiber having a PET core and a sheath made from a blend of granted HDPE and LLDPE in the wet laid web of the present invention again significantly increases the tensile strength value 200% of the values for the control while maintaining high tear strength and Mullen Burst value. The slightly lower

tear strength when compared to Experiment 2 is a further indication of superior bonding between the glass fibers and this bicomponent fiber.

Example 2

Thermally bonded wet laid webs were made up of varying amounts of bicomponent fibers and varying amounts of PET fibers used as matrix fibers. The webs were thermally bonded at 160°C. The thermally bonded webs were tested for strength, elongation and Mullen Burst. These values were compared to a wet laid web made up with a commercially available PET/HDPE bicomponent fiber (K-56) and varying amounts of PET matrix fiber.

In Experiments 1 A-D (the controls) a bicomponent fiber having a PET core and HDPE sheath as described in Example 1, Experiment 1, was used. The PET matrix fibers had a denier of 1.5 dpf and a cut length of 12,7 cm (0.5 inches).

Experiments 2 (A-D) were similar to Experiment 1, but the bicomponent fiber was replaced with bicomponent fiber B having a sheath core ratio of 40:60, a denier of 3 dpf, and a cut length of 0.5 inches.

Experiments 3 (A-C) were similar to Experiment 2 except the bicomponent fiber B had a sheath core ratio of 30:70.

Experiments 4 A-D were similar to Experiment 2, except the bicomponent fiber B had a sheath core ratio of 20:80.

The webs were tested for tensile strength, elongation Elmendorf tear strength and Mullen Burst values. The results of the Example are set forth in Table 2.

Table 2

		Bicomponent Fiber		PET Fiber		Strength		Elongation		Elmendorf Tear		Mullen Burst	
		(%)		(%)		(lb)	Kg	(%)	(%)	(lb)	Kg	(PSI)	KPa
Experiment 1 (control)	A	0		100		0.0	0	0.0		0.0	0	0.0	0
	B	20		80		0.4	0,18	2.7		0.7	0,315	8.0	55,2
	C	60		40		2.6	1,17	13.2		1.2	0,54	16.6	114,5
	D	100		0		8.6	3,87	37.7		1.7	0,765	35.0	241,5
Experiment 2	A	0		100		0.0	0	0.0		0.0	0	0.0	0
	B	20		80		2.4	1,08	5.5		0.9	0,405	19.0	131,1
	C	60		40		5.4	2,43	13.0		1.8	0,81	37.1	256
	D	100		0		7.7	3,47	24.7		1.6	0,72	30.0	207
Experiment 3	A	0		100		0.0	0	0.0		0.0	0	0.0	0
	B	30		70		5.8	4,0	3.1		0.8	0,36	13.3	92,8
	C	100		0		11.2	5	22.6		1.5		42.1	290,5
	A	0		100		0.0	0	0.0		0.0		0.0	0
Experiment 4	B	20		80		1.0	0,45	2.0		0.5	0,675	6.1	42,1
	C	60		40		3.9	2,7	5.2		1.2	0,54	25.7	177,3
	D	100		0		5.8	2,6	12.6		1.8	0,81	33.5	231,1

The results as shown in Table 2 are included in the graphs shown in Figures 1-4.

Experiments 1 A-D were the controls using a commercially available bicomponent fiber of a HDPE sheath and PET core. When only PET fiber is used in the wet lay, the web has no strength. At 60% bicomponent fiber, 40% PET matrix fiber, the web has only 2.6 lbs. of strength and a Mullen Burst value of 16.6.

Experiments 2 A-D demonstrates that by replacement of the HDPE/PET bicomponent fiber with bicomponent fiber B having a 40% sheath of the present invention, the strength of the web increases significantly as do the values for the Mullen Burst test.

Experiments 3 A-C demonstrates that by using the bicomponent fiber B having a 30% sheath, that 100% bicomponent fiber B web has a strength of 11.2 lbs., which is significantly higher than the Experiment 1-D.

Experiments 4 A-D demonstrates that using the bicomponent fiber B having only 20% sheath still results in a strength superior to that of the Experiment 1-C at 60% bicomponent: 40% PET fiber mix.

Example 3

Thermally bonded wet laid webs were made up of varying amounts of bicomponent fibers and PET fibers such that the total of the two fibers is 100%. The webs were thermally bonded at 370°F and were tested for tensile, elongation, Mullen Burst and tear.

Experiments 1, 2 and 3 were similar in that each contained 100% bicomponent fiber and no matrix fiber. Experiment 1 (control) contained a bicomponent fiber as described in Example 1, Experiment 1. Experiment 2 contained bicomponent fiber A and Experiment 3 contained bicomponent fiber B.

Experiments 4, 5 and 7 were similar in that each contained 75% bicomponent fiber and 25% PET fiber of 1.5 dpf and cut length of 1,27 cm (0.5 inches). Experiment 4 (control) contained the PET/HDPE bicomponent fiber; Experiment 5 contained bicomponent fiber A and Experiment 6 contained bicomponent fiber B.

Experiments 7, 8 and 9 each contained 50% bicomponent fiber and 50% PET fiber. Experiment 7 (control) contained the PET/HDPE bicomponent fiber; Experiment 8 contained bicomponent fiber A and Experiment 9 contained bicomponent fiber B.

Experiments 10, 11 and 12 each contained 25% bicomponent fiber and 75% PET fiber. Experiment 10 (control) contained the PET/HDPE bicomponent fiber; Experiment 11 contained bicomponent fiber A and Experiment 12 contained bicomponent fiber B.

The thermally bonded webs were tested for tensile strength, elongation, Elmendorf tear and Mullen Burst. The results of the test are set forth in Table 3.

Table 3

Experiments	Tensile		Elongation	Mullen Burst		Tear
		g/cm			kPa	
1	6.9	122,1	52.1	28.9	202,3	348.6
2	9.0	159,3	28.5	39.4	271,9	272.4
3	11.3	200,0	31.1	40.3	278,1	209.5
4	3.7	65,5	34.3	20.1	138,7	356.6
5	7.3	129,2	23.5	32.4	223,6	500.0
6	9.3	164,6	24.4	37.2	256,7	397.5
7	1.9	33,6	21.0	10.0	69	248.6
8	3.7	65,5	16.5	21.7	149,7	456.4
9	6.9	122,1	15.5	27.5	189,8	562.5
10	0.7	12,4	3.5	8.1	55,9	123.6
11	1.1	19,5	4.2	9.5	65,6	247.1
12	2.0	35,4	7.0	14.1	97,3	317.2

All webs thermally bonded at 370°F

All test results normalized to base weight

Tensile Values are in lbs/in

Tear values are in grams

Mullen test are in PSI

The control Experiments 1, 4, 7 and 10 each containing the PET/HDPE bicomponent fiber, have lower strengths as

demonstrated by the lower tensile and Mullen Burst values when compared to similar thermally bonded webs containing the bicomponent fibers of the present invention.

It is apparent that there has been provided in accordance with the invention, that the thermally bonded fibrous wet laid web and a method of preparing such a web incorporating a specific bicomponent fiber, fully satisfies the objects, aims and advantages as set forth above. While the invention has been described in conjunction with specific embodiments thereof, it is evident that many alternatives, modifications and variations will be apparent to those skilled in the art in light of the foregoing description.

Claims

1. A thermally bonded fibrous wet laid web consisting essentially of a bicomponent fiber comprising a first component of polyester or polyamide, and a second component comprising a linear low density polyethylene LLDPE copolymer having a density in the range of 0.88 to 0.945 g/cc, characterised in that the second component also comprises grafted high density polyethylene, HDPE, having initially a density in the range of 0.94 to 0.965 g/cc, which has been grafted with maleic acid or maleic anhydride, thereby providing succinic acid or succinic anhydride groups grafted along the HDPE polymer.
2. The thermally bonded fibrous wet laid web of claim 1 wherein the ratio of grafted HDPE: ungrafted LLDPE is in the range of 2:98 to 30:70.
3. The thermally bonded fibrous wet laid web of claim 1 or 2 wherein the melt flow value of the LLDPE polymer is in the range of 7 gm/10 min to 120 gm/10 min and the melt flow value of the grafted HDPE is in the range of 5 gm/10 min to 500 gm/10 min.
4. The thermally bonded fibrous wet laid web of claim 3 wherein the melt flow value of the LLDPE is in the range of 10 gm/10 min to 105 gm/10 min and the melt flow value of the grafted HDPE is in the range of 7 gm/10 min to 150 gm/10 min.
5. The thermally bonded fibrous wet laid web of any of claims 1-5 wherein the ungrafted LLDPE has a density in the range of 0.90 g/cc to 0.940 g/cc and has a C₄ - C₈ alkene comonomer content of 1% to 20% by weight of the LLDPE.
6. The thermally bonded fibrous wet laid web of claim 6 wherein the alkene comonomer comprises 1-octene.
7. The thermally bonded fibrous wet laid web of any of claims 1-5 wherein LLDPE copolymer has a density in the range of 0.88 g/cc to 0.945 g/cc and contains 0.5% to 35% by weight of a C₃ - C₁₂ alkene comonomer.
8. The thermally bonded fibrous wet laid web of claim 7 wherein the ungrafted LLDPE copolymer contains 2% to 15% by weight of 1-octene comonomer.
9. A thermally bonded fibrous wet laid web consisting essentially of a bicomponent fiber comprising a first component of polyester or polyamide; and a second component comprising linear low density polyethylene copolymer having density in the range of 0.88 to 0.945 g/cc; and a matrix fiber selected from the group consisting essentially of cellulose paper making fibers, cellulose acetate fibers, glass fibers, polyester fibers, metal fibers, mineral wool fibers, polyamide fibers and other naturally occurring fibers; characterised in that the second component also comprises grafted high density polyethylene, HDPE, having initially a density in the range of 0.94 to 0.965 g/cc, which has been grafted with maleic acid or maleic anhydride, thereby providing succinic acid or succinic anhydride groups grafted along the HDPE polymer chain.
10. The thermally bonded fibrous wet laid web of claim 9 wherein the ratio of grafted HDPE: ungrafted LLDPE is in the range of 2:98 to 30:70.
11. The thermally bonded fibrous wet laid web of claim 9 or 10 wherein the melt flow value of the LLDPE polymer is in the range of 7 gm/10 min to 120 gm/10 min and the melt flow value of the grafted HDPE is in the range of 5 gm/10 min to 500 gm/10 min.
12. The thermally bonded fibrous wet laid web of claim 11 wherein the melt flow value of the LLDPE is in the range of 10 gm/10 min to 105 gm/10 min and the melt flow value of the grafted HDPE is in the range of 7 gm/10 min to 150

gm/10 min.

13. The thermally bonded fibrous wet laid web of any of claims 9-12 wherein the LLDPE has a density in the range of 0.90 g/cc to 0.940 g/cc and has a C₄ - C₈ alkene comonomer content of 1% to 20% by weight of the LLDPE.
14. The thermally bonded fibrous wet laid web of claim 13 wherein the alkene comonomer comprises 1-octene.
15. The thermally bonded fibrous wet laid web of any of claims 9-12 wherein LLDPE copolymer is one having a density in the range of 0.88 g/cc to 0.945 g/cc containing 0.5% to 35% by weight of a C₃ - C₁₂ alkene comonomer.
16. The thermally bonded fibrous wet laid web of claim 15 wherein the LLDPE copolymer contains 2% to 15% by weight of 1-octene comonomer.
17. A thermally bonded fibrous wet laid web comprising a bicomponent fiber comprising a core of a polyester or polyamide; and a sheath consisting of linear low density polyethylene copolymer having a density in the range of 0.88 g/cc to 0.945 g/cc and grafted high density polyethylene, HDPE, having initially a density in the range of 0.94 to 0.965 g/cc, which has been grafted with maleic acid or maleic anhydride thereby providing succinic acid or succinic anhydride groups grafted along the HDPE polymer chain wherein the bicomponent fiber has a length to diameter ratio between 100:1 and 2,000:1; and a matrix fiber selected from the group consisting essentially of cellulose acetate fibers, glass fibers, polyester fibers, ceramic fibers, wool fibers, polyamide fibers, and other naturally occurring fibers.
18. A method of forming a thermally bonded fibrous wet laid web by wet laying fibers on paper making equipment or wet lay nonwoven equipment, the web comprising bicomponent fibers comprising a first component of polyester or polyamide, and a second component consisting essentially of linear low density polyethylene copolymer having a density in the range of 0.88 to 0.945 g/cc and grafted high density polyethylene, HDPE, having initially a density in the range of 0.94 to 0.965 g/cc, which has been grafted with maleic acid or maleic anhydride, thereby providing succinic acid or succinic anhydride groups grafted along the HDPE polymer; and matrix fibers wherein the steps of forming a fiber furnish by dispersion of said bicomponent fibers and matrix fibers in a carrier medium consisting essentially of water and a dispersant and a thickener, and supplying the fiber furnish at a consistency in the range of 0.01 to 0.5 weight percent fibers to the wire of a machine forming a fibrous web and then heating the fibrous web to melt the second component and thermally bond the fibrous web.

Patentansprüche

1. Thermisch verfestigter faseriger Naßvliesstoff, bestehend im wesentlichen aus einer Bikomponentenfaser, umfassend eine erste Komponente aus Polyester oder Polyamid und eine zweite Komponente, umfassend ein Copolymer aus linearem Polyethylen niedriger Dichte, LLDPE, mit einer Dichte im Bereich von 0,88 bis 0,945 g/cm³, dadurch gekennzeichnet, daß die zweite Komponente darüber hinaus gefropftes Polyethylen hoher Dichte, HDPE, umfaßt, das anfänglich eine Dichte im Bereich von 0,94 bis 0,965 g/cm³ aufweist, das mit Maleinsäure oder Maleinsäureanhydrid gefropft ist, wodurch Bernsteinsäure- oder Bernsteinsäureanhydridgruppen erhalten werden, die entlang des HDPE-Polymers gefropft sind.
2. Thermisch verfestigter faseriger Naßvliesstoff nach Anspruch 1, wobei das Verhältnis aus gefropftem HDPE : ungefropftem LLDPE im Bereich von 2 : 98 bis 30 : 70 liegt.
3. Thermisch verfestigter faseriger Naßvliesstoff nach Anspruch 1 oder 2, wobei der Schmelzflußwert des LLDPE-Polymers im Bereich von 7 g/10 min bis 120 g/10 min liegt und der Schmelzflußwert des gefropften HDPE im Bereich von 5 g/10 min bis 500 g/10 min liegt.
4. Thermisch verfestigter faseriger Naßvliesstoff nach Anspruch 3, wobei der Schmelzflußwert des LLDPE im Bereich von 10 g/10 min bis 105 g/10 min liegt und der Schmelzflußwert des gefropften HDPE im Bereich von 7 g/10 min bis 150 g/10 min liegt.
5. Thermisch verfestigter faseriger Naßvliesstoff nach einem der Ansprüche 1 bis 5, wobei das ungefropfte LLDPE eine Dichte im Bereich von 0,90 g/cm³ bis 0,940 g/cm³ aufweist und einen C₄-C₈-Alken-Comonomergehalt von 1 Gew.-% bis 20 Gew.-% des LLDPE aufweist.

6. Thermisch verfestigter faseriger Naßvliesstoff nach Anspruch 6, wobei das Alken-Comonomer 1-Octen umfaßt.
7. Thermisch verfestigter faseriger Naßvliesstoff nach einem der Ansprüche 1 bis 5, wobei das LLDPE-Copolymer eine Dichte im Bereich von 0,88 g/cm³ bis 0,945 g/cm³ aufweist und 0,5 Gew.-% bis 35 Gew.-% eines C₃-C₁₂-Alken-Comonomers aufweist.
8. Thermisch verfestigter faseriger Naßvliesstoff nach Anspruch 7, wobei das ungepfropfte LLDPE-Copolymer 2 Gew.-% bis 15 Gew.-% eines 1-Octen-Comonomers aufweist.
9. Thermisch verfestigter faseriger Naßvliesstoff, bestehend im wesentlichen aus einer Bikomponentenfaser, umfassend eine erste Komponente aus Polyester oder Polyamid und eine zweite Komponente, umfassend ein Copolymer aus linearem Polyethylen niedriger Dichte mit einer Dichte im Bereich von 0,88 bis 0,945 g/cm³; und einer Matrixfaser, ausgewählt aus der im wesentlichen aus Fasern zur Herstellung von Cellulosepapier, Celluloseacetat-Fasern, Glasfasern, Polyesterfasern, Metallfasern, Mineralwollefasern, Polyamidfasern und anderen natürlich vorkommenden Fasern bestehenden Gruppe; gekennzeichnet dadurch, daß die zweite Komponente darüber hinaus Polyethylen hoher Dichte, HDPE, umfaßt, das anfänglich eine Dichte im Bereich von 0,94 bis 0,965 g/cm³ aufweist, das mit Maleinsäure oder Maleinsäureanhydrid gepfropft ist, wodurch Bernsteinsäure- oder Bernsteinsäureanhydridgruppen erhalten werden, die entlang des HDPE-Polymers gepfropft sind.
10. Thermisch verfestigter faseriger Naßvliesstoff nach Anspruch 9, worin das Verhältnis aus gepfropftem HDPE : ungepfropftem LLDPE im Bereich von 2 : 98 bis 30 : 70 liegt.
11. Thermisch verfestigter faseriger Naßvliesstoff nach Anspruch 9 oder 10, wobei der Schmelzflußwert des LLDPE-Polymers im Bereich von 7 g/10 min bis 120 g/10 min liegt und der Schmelzflußwert des gepfropften HDPE im Bereich von 5 g/10 min bis 500 g/10 min liegt.
12. Thermisch verfestigter faseriger Naßvliesstoff nach Anspruch 11, wobei der Schmelzflußwert des LLDPE-Polymers im Bereich von 10 g/10 min bis 105 g/10 min liegt und der Schmelzflußwert des gepfropften HDPE im Bereich von 7 g/10 min bis 150 g/10 min liegt.
13. Thermisch verfestigter faseriger Naßvliesstoff nach einem der Ansprüche 9 bis 12, wobei das LLDPE eine Dichte im Bereich von 0,90 g/cm³ bis 0,940 g/cm³ aufweist und einen C₄-C₈-Alken-Comonomergehalt von 1 Gew.-% bis 20 Gew.-% des LLDPE aufweist.
14. Thermisch verfestigter faseriger Naßvliesstoff nach Anspruch 13, wobei das Alken-Comonomer 1-Octen umfaßt.
15. Thermisch verfestigter faseriger Naßvliesstoff nach einem der Ansprüche 9 bis 12, wobei das LLDPE-Copolymer eine Dichte im Bereich von 0,88 g/cm³ bis 0,945 g/cm³ aufweist, das 0,5 Gew.-% bis 35 Gew.-% eines C₃-C₁₂-Alken-Comonomers aufweist.
16. Thermisch verfestigter faseriger Naßvliesstoff nach Anspruch 15, wobei das LLDPE-Copolymer 2 Gew.-% bis 15 Gew.-% eines 1-Octen-Comonomers aufweist.
17. Thermisch verfestigter faseriger Naßvliesstoff, umfassend eine Bikomponentenfaser, umfassend einen Kern aus einem Polyester oder Polyamid und einen Mantel, bestehend aus einem Copolymer aus linearem Polyethylen niedriger Dichte mit einer Dichte im Bereich von 0,88 bis 0,945 g/cm³, und Polyethylen hoher Dichte, HDPE, das anfänglich eine Dichte im Bereich von 0,94 bis 0,965 g/cm³ aufweist, das mit Maleinsäure oder Maleinsäureanhydrid gepfropft ist, wodurch Bernsteinsäure- oder Bernsteinsäureanhydridgruppen erhalten werden, die entlang der HDPE-Polymerkette gepfropft sind, wobei die Bikomponentenfaser ein Verhältnis von Länge zu Durchmesser zwischen 100 : 1 und 2000 : 1 aufweist; und eine Matrixfaser, ausgewählt aus der im wesentlichen aus Celluloseacetat-Fasern, Glasfasern, Polyesterfasern, keramischen Fasern, Wollfasern, Polyamidfasern und anderen natürlich vorkommenden Fasern bestehenden Gruppe.
18. Verfahren zur Bildung eines thermisch verfestigten faserigen Naßvliesstoffs durch das Naßverlegen von Fasern auf einer Apparatur zur Herstellung von Papier oder einer Naßvliesstoff-Apparatur, wobei das Vlies Bikomponentenfaser umfaßt, umfassend eine erste Komponente aus Polyester oder Polyamid und eine zweite Komponente, bestehend im wesentlichen aus einem Copolymer aus linearem Polyethylen niedriger Dichte mit einer Dichte im Bereich von 0,88 bis 0,945 g/cm³ und einem gepfropften Polyethylen hoher Dichte, HDPE, das anfänglich eine Dichte im

Bereich von 0,94 bis 0,965 g/cm³ aufweist, das mit Maleinsäure oder Maleinsäureanhydrid gefropft ist, wodurch Bernsteinsäure- oder Bernsteinsäureanhydridgruppen erhalten werden, die entlang des HDPE-Polymers gefropft sind; und Matrixfasern, umfassend die Schritte des Bildens eines Faserrohstoffs durch das Dispergieren der Bikomponentenfasern und der Matrixfasern in einem im wesentlichen aus Wasser und einem Dispergiemittel und einem Verdickungsmittel bestehenden Trägermedium und des Zuführens des Faserrohstoffs bei einer Konsistenz im Bereich von 0,01 bis 0,5 Gew.-% Fasern zum Draht einer Maschine, die eine Faserbahn bildet, und dann des Erwärms der Faserbahn, wodurch die zweite Komponente geschmolzen und die Faserbahn thermisch verfestigt wird.

Revendications

1. Nappe fibreuse liée thermiquement, établie par voie humide, consistant essentiellement en une fibre à deux composants comprenant un premier composant polyester ou polyamide et un second composant comprenant un copolymère de polyéthylène linéaire basse densité, PELBD, ayant une masse volumique comprise dans la plage de 0,88 à 0,945 g/cm³, caractérisée en ce que le second composant comprend aussi un polyéthylène haute densité, PEHD, greffé, ayant initialement une masse volumique comprise dans la plage de 0,94 à 0,965 g/cm³, qui a été greffé avec de l'acide maléique ou de l'anhydride maléique de manière qu'il présente des groupes acide succinique ou anhydride succinique greffé le long du polymère PEHD.
2. Nappe fibreuse liée thermiquement établie par voie humide suivant la revendication 1, dans laquelle le rapport du PEHD greffé au PELBD non greffé est compris dans la plage de 2:98 à 30:70.
3. Nappe fibreuse liée thermiquement établie par voie humide suivant la revendication 1 ou 2, dans laquelle l'indice d'écoulement à l'état fondu du polymère PELBD se situe dans la plage de 7 g/10 min à 120 g/10 min et l'indice d'écoulement à l'état fondu du PEHD greffé se situe dans la plage de 5 g/10 min à 500 g/10 min.
4. Nappe fibreuse liée thermiquement établie par voie humide suivant la revendication 3, dans laquelle l'indice d'écoulement à l'état fondu du PELBD se situe dans la plage de 10 g/10 min à 105 g/10 min et l'indice d'écoulement à l'état fondu du PEHD greffé se situe dans la plage de 7 g/10 min à 150 g/10 min.
5. Nappe fibreuse liée thermiquement établie par voie humide suivant l'une quelconque des revendications 1 à 4, dans laquelle le PELBD non greffé a une masse volumique comprise dans la plage de 0,90 g/cm³ à 0,940 g/cm³ et a une teneur en comonomère alcénique en C₄ à C₈ de 1 à 20 % en poids du PELBD.
6. Nappe fibreuse liée thermiquement établie par voie humide suivant la revendication 5, dans laquelle le comonomère alcénique comprend du 1-octène.
7. Nappe fibreuse liée thermiquement établie par voie humide suivant l'une quelconque des revendications 1 à 5, dans laquelle le copolymère PELBD a une masse volumique comprise dans la plage de 0,88 g/cm³ à 0,945 g/cm³ et contient 0,5 à 35 % en poids de comonomère alcénique en C₃ à C₁₂.
8. Nappe fibreuse liée thermiquement établie par voie humide suivant la revendication 7, dans laquelle le copolymère PELBD non greffé contient 2 à 15 % en poids de 1-octène comonomère.
9. Nappe fibreuse liée thermiquement établie par voie humide consistant essentiellement en une fibre à deux composants comprenant un premier composant polyester ou polyamide ; et un second composant comprenant un copolymère de polyéthylène linéaire basse densité ayant une masse volumique comprise dans la plage de 0,88 à 0,945 g/cm³; et une matrice de fibres choisies dans le groupe consistant essentiellement en fibres cellulosiques de fabrication du papier, fibres d'acétate de cellulose, fibres de verre, fibres de polyester, fibres métalliques, fibres de laine minérale, fibres de polyamide ou autres fibres naturelles ; caractérisée en ce que le second composant comprend aussi un polyéthylène haute densité, PEHD, greffé, ayant initialement une masse volumique comprise dans la plage de 0,94 à 0,965 g/cm³ qui a été greffé avec de l'acide maléique ou de l'anhydride maléique, de manière que des groupes acide succinique ou anhydride succinique soient présents le long de la chaîne de polymère PEHD.
10. Nappe fibreuse liée thermiquement établie par voie humide suivant la revendication 9, dans laquelle le rapport du PEHD greffé au PELBD non greffé se situe dans la plage de 2:98 à 30:70.

11. Nappe fibreuse liée thermiquement établie par voie humide suivant la revendication 9 ou 10, dans laquelle l'indice d'écoulement à l'état fondu du polymère PELBD se situe dans la plage de 7 g/10 min à 120 g/10 min et l'indice d'écoulement à l'état fondu du PEHD greffé se situe dans la plage de 5 g/10 min à 500 g/10 min.

5 12. Nappe fibreuse liée thermiquement établie par voie humide suivant la revendication 11, dans laquelle l'indice d'écoulement à l'état fondu du PELBD se situe dans la plage de 10 g/10 min à 105 g/10 min et l'indice d'écoulement à l'état fondu du PEHD greffé se situe dans la plage de 7 g/10 min à 150 g/10 min.

10 13. Nappe fibreuse liée thermiquement établie par voie humide suivant l'une quelconque des revendications 9 à 12, dans laquelle le PELBD a une masse volumique comprise dans la plage de 0,90 g/cm³ à 0,940 g/cm³ et une teneur en comonomère alcénique en C₄ à C₈ de 1 à 20 % en poids du PELBD.

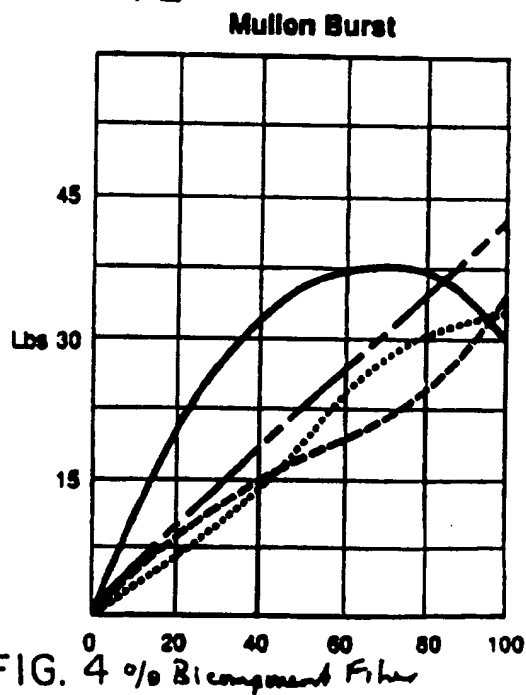
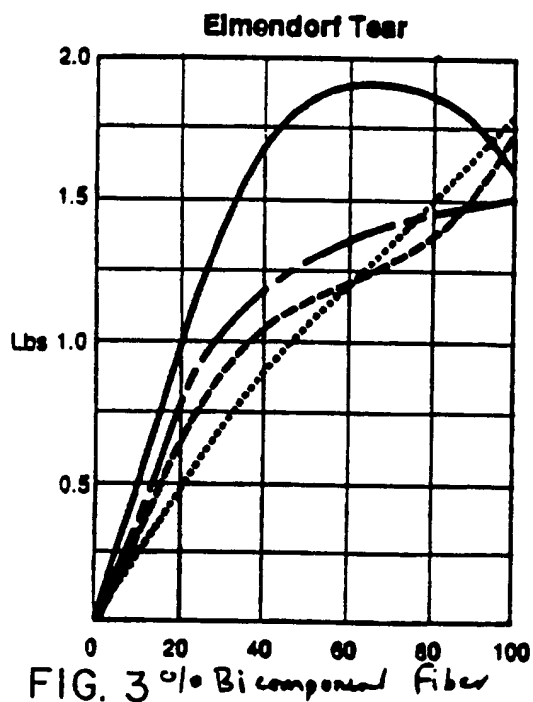
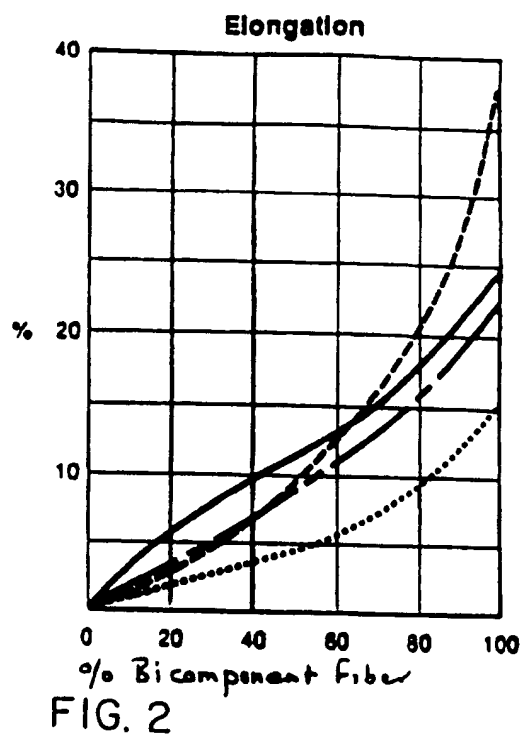
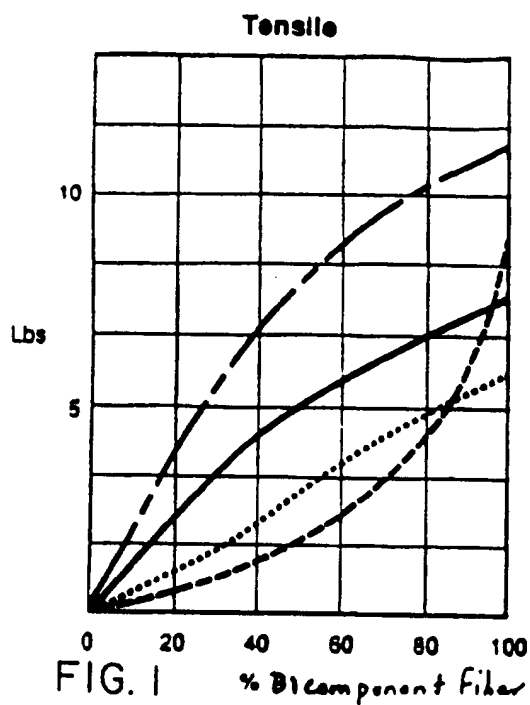
15 14. Nappe fibreuse liée thermiquement établie par voie humide suivant la revendication 13, dans laquelle le comonomère alcénique comprend du 1-octène.

15. Nappe fibreuse liée thermiquement établie par voie humide suivant l'une quelconque des revendications 9 à 12, dans laquelle le copolymère PELBD est un copolymère ayant une masse volumique comprise dans la plage de 0,88 g/cm³ à 0,945 g/cm³ contenant 0,5 à 35 % en poids d'un comonomère alcénique en C₃ à C₁₂.

20 16. Nappe fibreuse liée thermiquement établie par voie humide suivant la revendication 15, dans laquelle le copolymère PELBD contient 2 à 15 % en poids de 1-octène comme comonomère.

25 17. Nappe fibreuse liée thermiquement établie par voie humide comprenant une fibre à deux composants comportant un noyau en un polyester ou polyamide ; et une gaine consistant en un copolymère de polyéthylène linéaire basse densité ayant une masse volumique comprise dans la plage de 0,88 g/cm³ à 0,945 g/cm³ et un polyéthylène haute densité, PEHD, greffé, ayant initialement une masse volumique comprise dans la plage de 0,94 à 0,965 g/cm³, qui a été greffé avec de l'acide maléique ou de l'anhydride maléique de manière que des groupes acide succinique ou anhydride succinique soient présents à l'état greffé le long de la chaîne du polymère PEHD, la fibre à deux composants ayant un rapport longueur:diamètre compris entre 100:1 et 2000:1 ; et une matrice de fibres choisies dans le groupe essentiellement constitué de fibres d'acétate de cellulose, de fibres de verre, de fibres de polyester, de fibres céramiques, de fibres de laine, de fibres de polyamide et d'autres fibres naturelles.

35 18. Procédé pour établir par voie humide une nappe fibreuse liée thermiquement par dépôt de fibres par voie humide sur une installation de fabrication de papier ou une installation de fabrication d'un non-tissé établi par voie humide, la bande comprenant des fibres à deux composants comportant un premier composant de polyester ou polyamide et un second composant consistant essentiellement en un copolymère de polyéthylène linéaire basse densité ayant une masse volumique comprise dans la plage de 0,88 à 0,945 g/cm³ et un polyéthylène haute densité, PEHD, greffé ayant initialement une masse volumique comprise dans la plage de 0,94 à 0,965 g/cm³, qui a été greffé avec de l'acide maléique ou de l'anhydride maléique de manière que des groupes acide succinique ou anhydride succinique soient présents à l'état greffé le long du polymère PEHD ; et une matrice de fibres, comprenant les étapes de formation d'une charge fibreuse par dispersion des fibres à deux composants et des fibres formant la matrice dans un véhicule consistant essentiellement en eau contenant un dispersant et un agent épaississant, et l'amenée de la charge fibreuse, à une consistance comprise dans la plage de 0,01 à 0,5 % en poids de fibres, à la toile métallique d'une machine de formation d'une nappe fibreuse, puis chauffage de la nappe fibreuse, pour faire fondre le second composant et pour lier thermiquement la nappe fibreuse.



----- Control (50% Sheath)
 - - - - - Bi component A (30% Sheath)

————— Bi component B (40% Sheath)
 Bi component B (20% Sheath)